

Code No: 09A60305

JAWAHARLAL NEHRU TECHNOLOGICAL UNIVERSITY, HYDERABAD

B. Tech III Year II Semester Examinations, June-2014

**HEAT TRANSFER**

(Common to AME, ME)

Time: 3 hours

Max. Marks: 75

Answer any five questions  
All questions carry equal marks

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- 1.a) Derive differential equation of heat conduction in Cylindrical coordinate system?
- b) A hot plate of length 0.75 m, width 0.5m, and thickness 2 cm is placed in air stream at 20°C. It is estimated that a total of 300 W is lost from the plate surface by radiation. Taking the convective heat transfer coefficient as 25 W/m<sup>2</sup>K, and thermal conductivity of the plate as 43 W/mK, calculate the inside temperature of the plate?
- 2.a) Derive the expression for efficiency and effectiveness of rectangular fins?
- b) Triangular fins 2.5 cm thickness at base and 10 cm long and made from stainless steel ( $k = 17.7 \text{ W/mK}$  and  $\rho = 7850 \text{ kg/m}^3$ ) are to be fitted to an air cooled cylinder wall. If the wall temperature is 6 °C and the heat transfer coefficient between the solid surface and air ( $T_\infty = 40 \text{ °C}$ ) is 20 W/m<sup>2</sup>K, derive an expression for temperature distribution along the fin. Also estimate the rate of heat flow per unit mass of the fin.
- 3.a) Determine thermal diffusivity. Explain its significance in terms of penetration depth for a semi infinite body.
- b) A slab of aluminium 10 cm thick is originally in a temperature of 500 °C. It is suddenly immersed in a liquid at 100 °C resulting in a heat transfer coefficient of 1200 W/m<sup>2</sup>K. Determine the temperature at the center line and the surface 1 minute after the immersion. Also calculate the total thermal energy removed per unit area of the slab during this period. The properties of aluminium for the given conditions are
- $$\alpha = 8.4 \times 10^{-5} \text{ m}^2/\text{s} \quad k = 215 \text{ W/mK}$$
- $$\rho = 2700 \text{ kg/m}^3 \quad c = 0.9 \text{ kJ/kg/K}$$
- 4.a) What is Prandtl number? Show that it is a dimensionless quantity?
- b) Air at a pressure of 8 kN/m<sup>2</sup> and a temperature at 250 °C flows over a flat plate 0.3 m wide and 1 m long at a velocity of 8 m/s. If the plate is to be maintained a temperature of 78°C estimate the rate of heat to be removed continuously from the plate?

- 5.a) Using dimensional analysis establish a relation between Nusselt, Prandtl and Grashof number?
- b) A 30 cm long glass plate is hung vertically in the air at 27°C while its temperature is maintained at 77°C. Calculate the boundary layer thickness at the trailing edge of the plate. If a similar plate is placed in a wind tunnel and air is blown over it at a velocity of 4 m/s, estimate the boundary layer thickness at its trailing edge.
- 6.a) Distinguish between filmwise and dropwise condensation. Which of the two gives a higher heat transfer coefficient? Why?
- b) Determine the stable film boiling heat transfer coefficient for the film boiling of saturated water at atmospheric pressure on an electrically heated 1.6 mm diameter horizontal platinum wire with a temperature difference  $T_s - T_{sat} = 225^\circ\text{C}$ . What would be power dissipation per unit length of the heater?
- 7.a) Discuss the general arrangement of parallel flow, counter flow and cross flow heat exchangers? And why a counter flow heat exchanger more effective than a parallel flow exchanger?
- b) Water enters a counter flow, double pipe heat exchanger at 15°C, flowing at the rate of 1300 kg/h. It is heated by oil ( $C_p = 2 \text{ J/kg.K}$ ) flowing at the rate of 550 kg/h from the inlet temperature of 94°C. For an area of  $1 \text{ m}^2$  an overall heat transfer coefficient of  $1075 \text{ W/m}^2.\text{K}$ , determine the total heat transfer and the outlet temperatures of water and oil?
- 8.a) Distinguish between:
- A black body and gray body
  - Specular and diffuse surfaces
  - Absorptivity and emissivity of a surface
  - Total emissivity and equilibrium emissivity.
- b) A pipe carrying steam having an outside diameter 20 cm runs in a large room, and is exposed to air at a temperature of 30°C. The pipe surface temperature is 200°C. Find the heat loss per metre length of the pipe by convection and radiation taking the emissivity of the pipe surface as 0.8.

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